

Densities and Viscosities of Rubidium Bromide in Dimethyl Sulfoxide + Water Mixtures in the Temperature Range $t = (25 \text{ to } 45) \text{ }^\circ\text{C}$. Talat Zamir, S. Tasleem, Fahim Uddin,* and Shaheen Durrani, *J. Chem. Eng. Data* **2010**, 55, 666–672.

In the second column of Table 2 of the original paper, the density values of RbBr in dimethyl sulfoxide (1) + water (2)

Table 2

RbBr $t = 30 \text{ }^\circ\text{C}$	
$w_1 = 1.0$	
$c/\text{mol}\cdot\text{dm}^{-3}$	$\rho/\text{g}\cdot\text{cm}^{-3}$
0.011	1.09554
0.020	1.09751
0.026	1.09901
0.030	1.10033
0.056	1.10093

at $t = 30 \text{ }^\circ\text{C}$ are reported. Because of a typographical error, these data are wrong.

The authors apologize for this mistake.

JE1002847

10.1021/je1002847

Published on Web 04/26/2010

Vapor–Liquid Equilibria in Binary Systems Formed by n -Hexane with Alcohols. Paweł Gierycz,* Andrzej Kosowski, and Ryszard Swietlik, *J. Chem. Eng. Data* **2010**, 55, 937–940.

In the original version of this article that was published on the Web on November 23, 2009, two files were inadvertently included as Supporting Information. In the corrected version that was reposted on April 15, 2010, these files and the Supporting Information Available paragraph have been removed.

JE100340Y

10.1021/je100340y

Published on Web 04/15/2010

Density, Refractive Index, Speed of Sound at 298.15 K, and Vapor–Liquid Equilibrium at 101.3 kPa for Binary Mixtures of Methanol + Ethyl Lactate and 1-Propanol + Ethyl Lactate. José M. Resa,* Emilio A. Cepeda, José M. Goenaga, Álvaro Ramos, Sofía Aguirre, and Cipriano Urbano, *J. Chem. Eng. Data* **2010**, 55, 1017–1021.

On page 1019, the data in Table 5 are incorrect. The problem was that if $T = f(x)$ was plotted with the data in Table 5, one did not get the bubble temperature curve (lower curve) in Figure 2. The plot of the $y = f(x)$ curve is acceptable.

The correct values are given below in the new Table 5.

Table 5. Experimental VLE Data for the Binary 1-Propanol (1) + Ethyl Lactate (2) System at 101.33 kPa

x_1	y_1	T/K	γ_1	γ_2
0.000	0.000	427.60		
0.008	0.070	425.35	1.69	1.00
0.022	0.162	422.25	1.54	1.00
0.033	0.224	419.85	1.50	1.01
0.045	0.284	417.45	1.48	1.01
0.079	0.419	412.05	1.44	1.00
0.169	0.622	401.95	1.32	0.99
0.206	0.665	399.35	1.25	1.00
0.239	0.700	397.15	1.21	1.01
0.275	0.732	394.75	1.18	1.02
0.310	0.759	392.65	1.16	1.04
0.340	0.789	390.25	1.18	1.03
0.408	0.820	387.45	1.12	1.08
0.438	0.843	385.85	1.13	1.05
0.522	0.878	382.85	1.09	1.07
0.625	0.908	379.65	1.05	1.15
0.701	0.932	377.65	1.02	1.15
0.750	0.942	376.35	1.01	1.23
0.836	0.970	374.15	1.01	1.05
0.935	0.988	371.75	1.00	1.21
1.000	1.000	370.4		

Acknowledgment

We thank Dr. Chirico of NIST for pointing out the problem.

JE1002219

10.1021/je1002219

Published on Web 04/13/2010